



# **Future of Membrane Technology in Worldwide Sanitation**

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# This Presentation

- **Premise**
  - Membranes-based processes are the best available technologies for wastewater treatment and reuse
    - MF/UF for tertiary filtration or MBR
    - RO for desalination or polishing
- **Objective**

Establish gaps in current knowledge / products / practices
- **Approach**

Identify key issues on selected topics

# Selected Topics

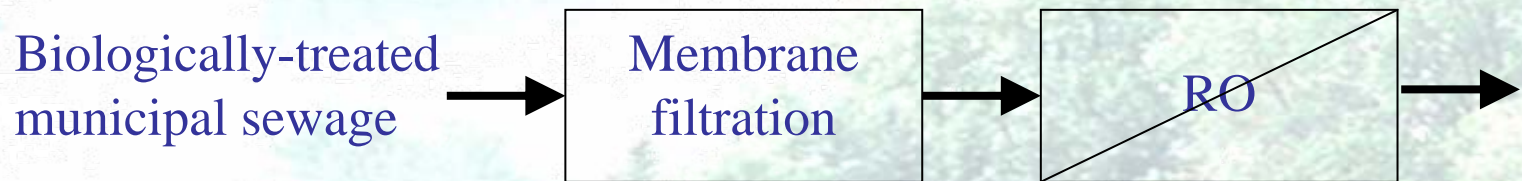
- 1) Water reuse versus seawater desalination
- 2) Tertiary filtration versus membrane bioreactor
- 3) Pressurized versus immersed membranes
- 4) MF/UF and RO pre-treatment
- 5) Flux and fouling
- 6) MBR pre-treatment
- 7) The use of air with membranes
- 8) Handling residuals

# 1) Water Reuse vs Seawater Desalination

- Sewage is the only abundant source of water present wherever there are people...
- For environmental sustainability, sewage needs to be treated biologically for discharge
- The incremental cost for reuse is a fraction of the cost of seawater desalination
- The main adoption barrier is not technical, but public acceptability...

# Water Reuse vs Seawater Desalination

## Water Reuse



## Seawater Desalination



# Process Design Conditions for the Comparison of Water Reuse and Desalination

| Unit process          | Parameter              | Units               | Water Reuse            | Desalination           |
|-----------------------|------------------------|---------------------|------------------------|------------------------|
| Coagulation           | FeCl <sub>3</sub> dose | mg/L                | No                     | 5                      |
| Pretreatment          |                        |                     | MBR or CAS-TF effluent | Multi media filtration |
| Anti-scalant addition | Dose                   | mg/L                | 2                      | 5                      |
| Reverse Osmosis       | Stages                 | Number              | 1                      | 2                      |
|                       | Recovery               | %                   | >80                    | <50                    |
|                       | Flux                   | L/m <sup>2</sup> /h | 20                     | 14                     |
|                       | Feed pressure          | bar                 | 13.6                   | 54                     |

# Costs of Producing Water from Secondary Effluent and from Seawater

| <b>Component</b>              | <b>Units</b>         | <b>A: from<br/>CAS<br/>effluent</b> | <b>B: from<br/>seawater</b> | <b>Ratio<br/>(B/A)</b> |
|-------------------------------|----------------------|-------------------------------------|-----------------------------|------------------------|
| <b>Capital costs</b>          |                      |                                     |                             |                        |
| Infrastructure & pretreatment | \$/m <sup>3</sup> /d | 161                                 | 320                         | 1.99                   |
| RO                            | \$/m <sup>3</sup> /d | 321                                 | 624                         | 1.94                   |
| <b>Total</b>                  | \$/m <sup>3</sup> /d | <b>482</b>                          | <b>944</b>                  | <b>1.96</b>            |
| <b>Total Life cycle costs</b> |                      |                                     |                             |                        |
| Capital                       | \$/m <sup>3</sup>    | 0.07                                | 0.24                        | 3.43                   |
| O&M                           | \$/m <sup>3</sup>    | 0.21                                | 0.38                        | 1.81                   |
| <b>Total</b>                  | \$/m <sup>3</sup>    | <b>0.28</b>                         | <b>0.62</b>                 | <b>2.21</b>            |

## 2) Tertiary Filtration of CAS versus MBR

### Tertiary Filtration

- Conventional activated sludge plant exists
- Discharge requirements are met
- WW flow is highly variable
- Reused water needs are seasonal
- Reused water flow rate is a small portion of the total flow rate
- Flux limited by fouling

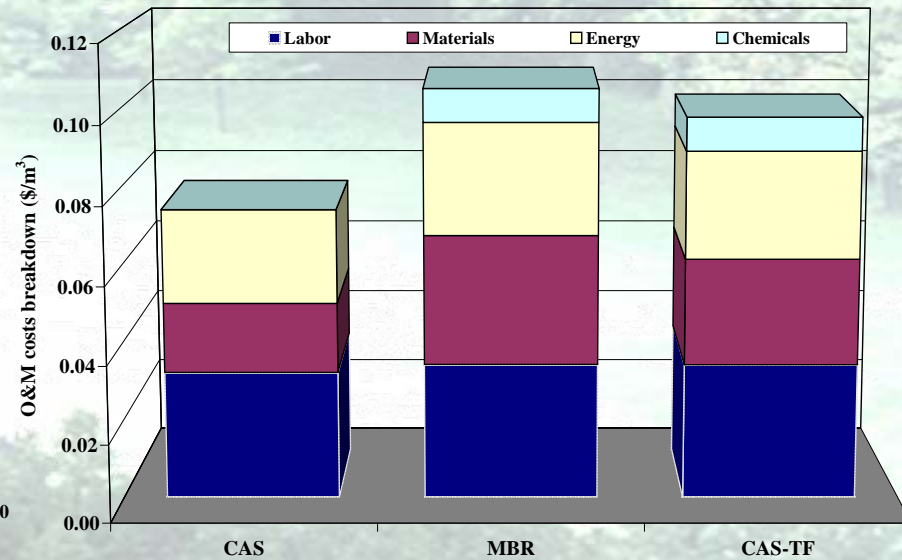
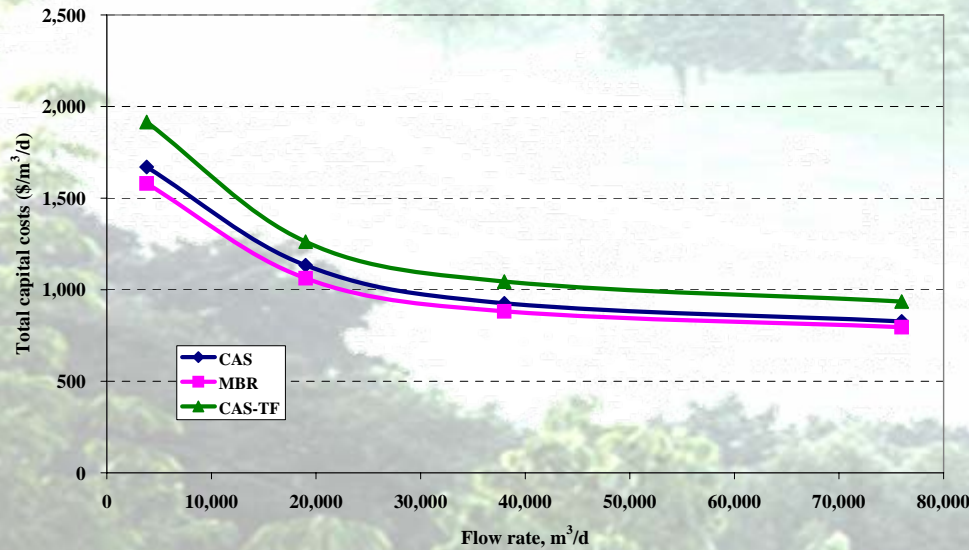
### Membrane Bioreactor

- New plant
- Stringent discharge requirements
- Low peaking factors
- Large fraction of volume treated is reused
- Flux limited by solids handling
- Pre-treatment critical to protect the membranes



# Cost Comparison of CAS, Tertiary Filtration and MBR

- Capital costs of MBR are lower
- O&M cost of MBR are larger
- Overall, there is a 10-15% premium over CAS for adding a membrane step



### 3) Pressurized versus Immersed Membranes

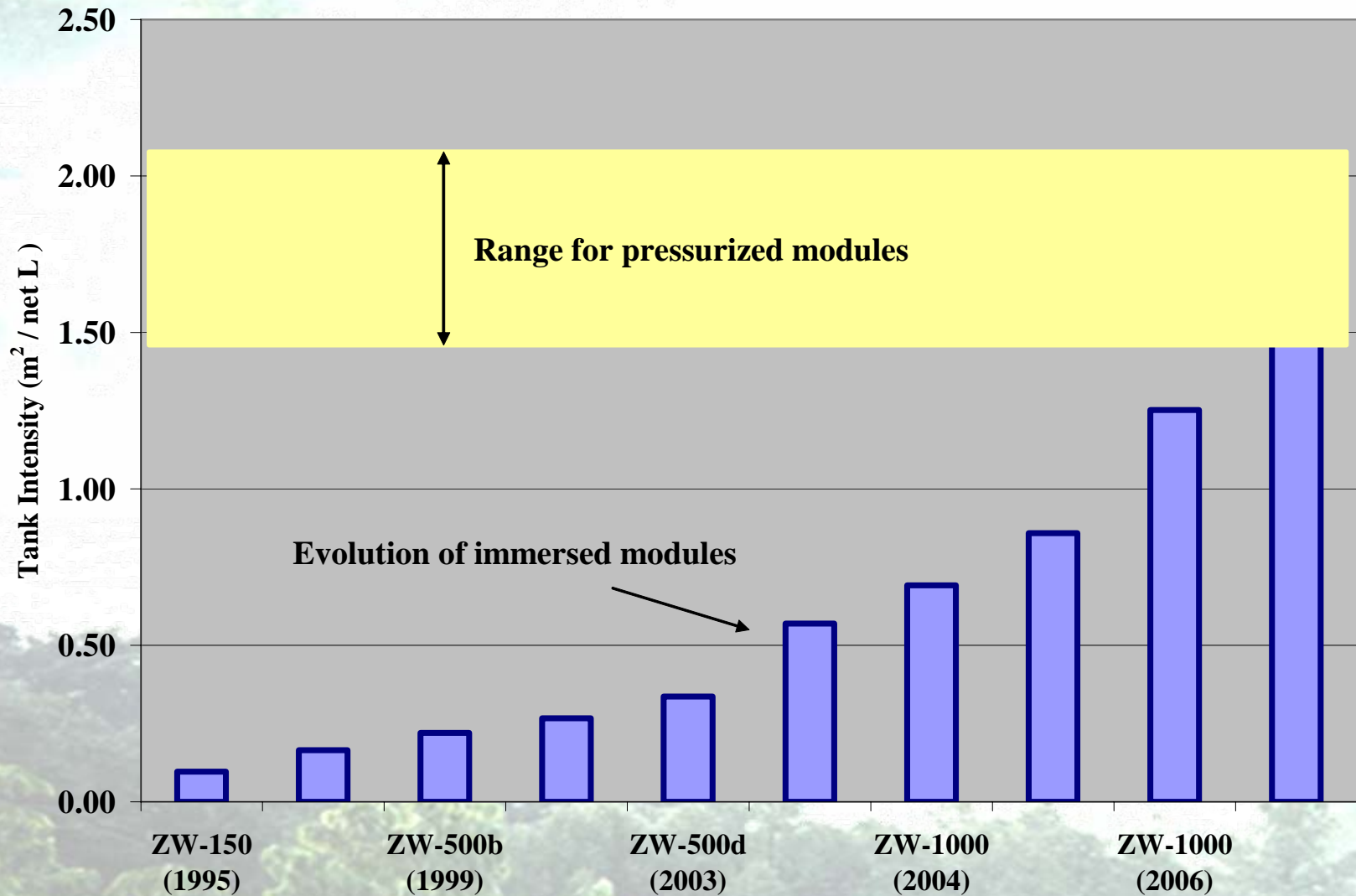
#### Pressurized

- I/O or O/I; cost penalty ( $\approx 40\%$ ) for I/O difficult to overcome
- Higher TMP possible is a benefit for low fouling water
- Air essential for cleaning in O/I configuration
- Cost benefits for smaller systems

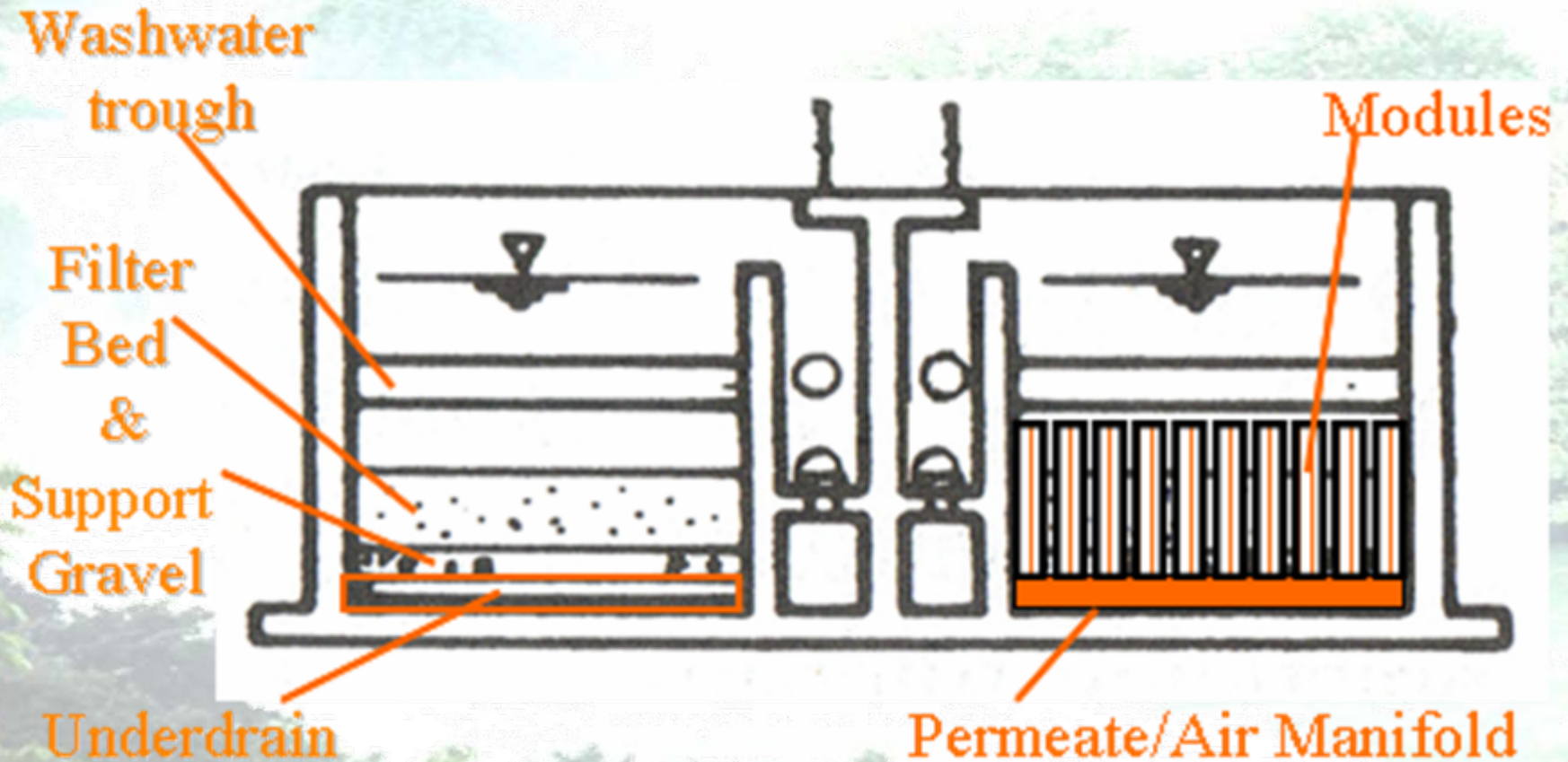
#### Immersed

- Only O/I
- Lower TMP and flux are benefits for high fouling water
- Packing density penalty disappearing...
- Easier scale-up makes it better for large scale systems

# Evolution of Immersed Membranes



# Can Immersed Membranes be Used in a Simple Sand Filter Retrofit?



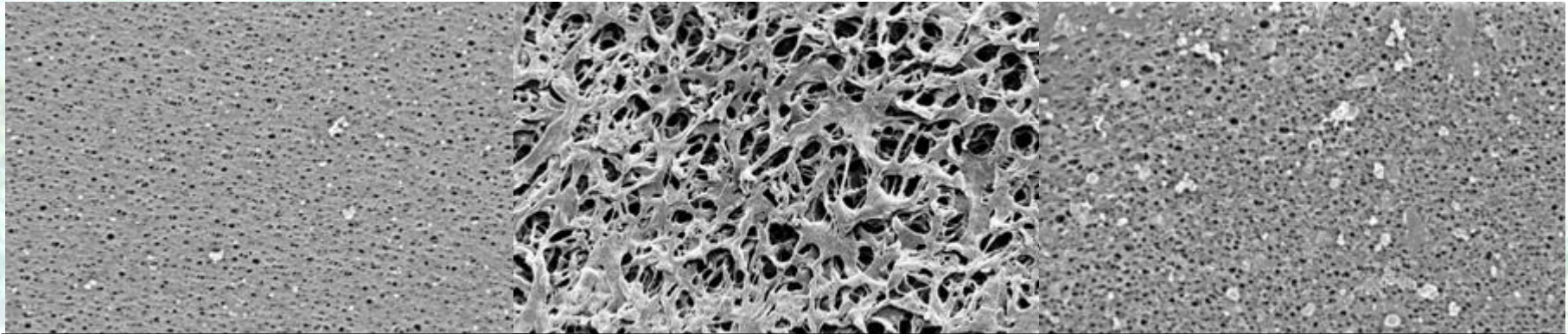
## 4) MF/UF as RO Pre-treatment

- Best pre-treatment for particles and colloids
- May increase the rate of organic fouling when compared to coagulation / filtration
- Does little to protect against bio-fouling or scaling
- Does MF/UF pre-treatment increase the risk of RO membrane damage by chlorine?
- Can RO modules / systems be optimized for use with MF/UF pre-treatment?
- How to best integrate an interrupted process (MF/UF) with a continuous process (RO)?

# 5) Balance between Flux and Fouling

- Current project evaluation criteria favour higher flux (are the consequences of frequent cleaning properly evaluated?)
- Membranes with a large number of small pores are better...
- Biggest manufacturers challenge is to develop permanently hydrophilic membranes
- Fouling in seawater is not well understood
- What is the best approach to improve the filterability of MBR sludge?

# Importance of Membrane Morphology

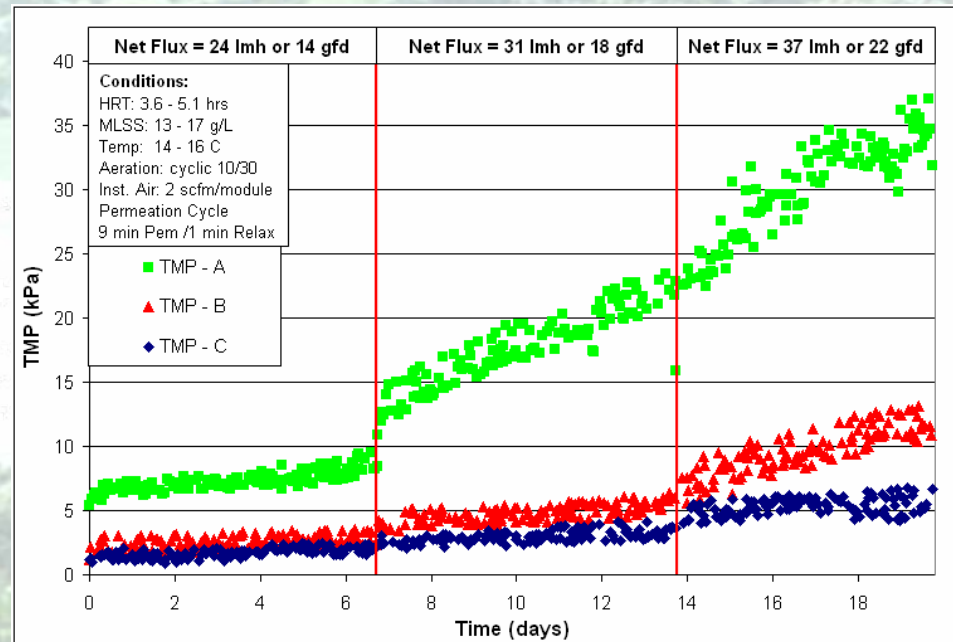


**A (100kx): 0.04  $\mu\text{m}$   
300 Lmh/bar**

**B (20kx): 0.4  $\mu\text{m}$   
1500 Lmh/bar**

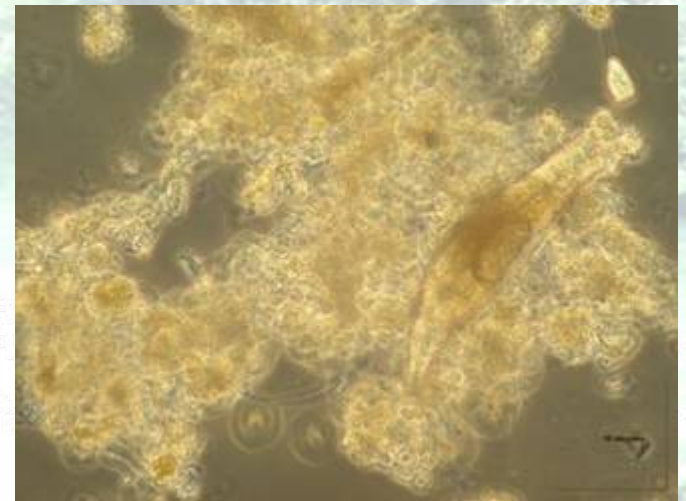
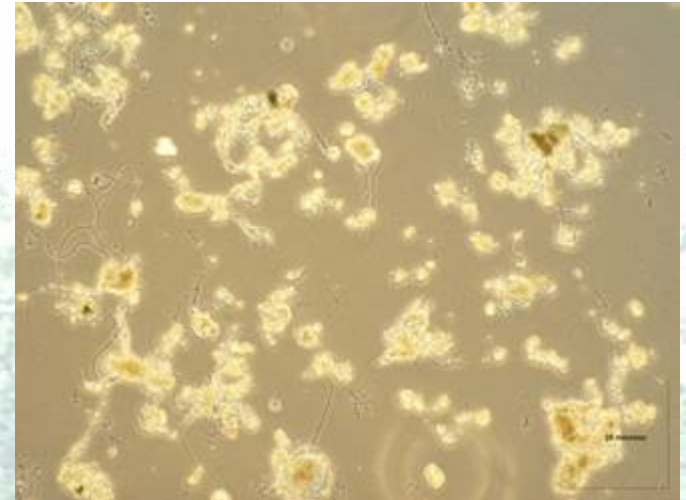
**C (100kx): 0.04  $\mu\text{m}$   
1000 Lmh/bar**

Large number of small pores allows high permeability and prevents deep membrane fouling



# How to Enhance MBR Sludge Filterability

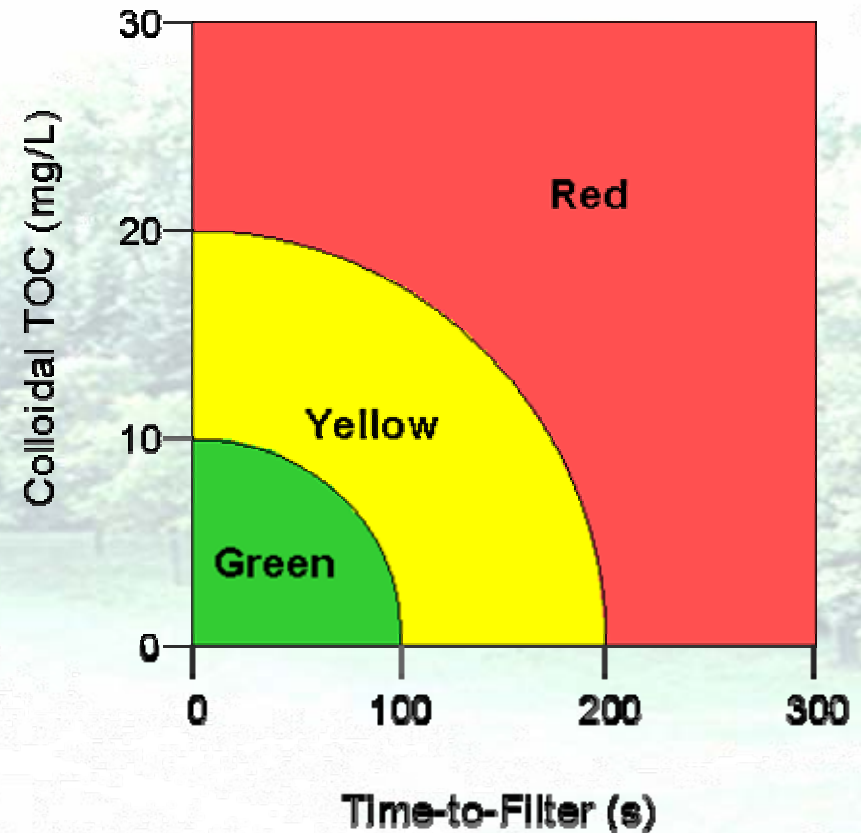
1. Ensure complete nitrification (SRT > 12-d)
2. Avoid extra long SRT that results in entrapment of colloids in the ML
3. Maintain DO > 1-mg/L in the membrane tank
4. Provide minimum HRT of 2-hours between feed addition point and membranes
5. Use low shear RAS pumps
6. Avoid sudden changes in environmental conditions (pH, loading, etc.)





# Sludge Filterability

| Mixed Liquor Property  | Significance                                       | Method                  |
|--|--|-------------------------|
| Hydraulic permeability of the cake layer formed from large flocs | Dominates in low shear membrane filtration system  | Modified Time-to-Filter |
| Pore-plugging potential of interstitial colloidal particles      | Dominates in high shear membrane filtration system | Colloidal TOC           |



## 6) MBR Pre-treatment

- Sewage contains 10-20 mg/L of trash that can be concentrated by a factor of 50-100 in a MBR (SRT/HRT)
- Impacts of poor pretreatment include reduction in hydraulic capacity, degradation of effluent quality, increase in O&M costs, reduction in membrane life
- Designing modules to handle trash leads to sub-optimal performance...
- Fine head-works screening represents only 3% of the total investment cost for a MBR
- Mixed liquor screening is an option to fully protect the membranes and eliminate the generation screenings as a separate waste stream

# Importance of MBR Pretreatment...

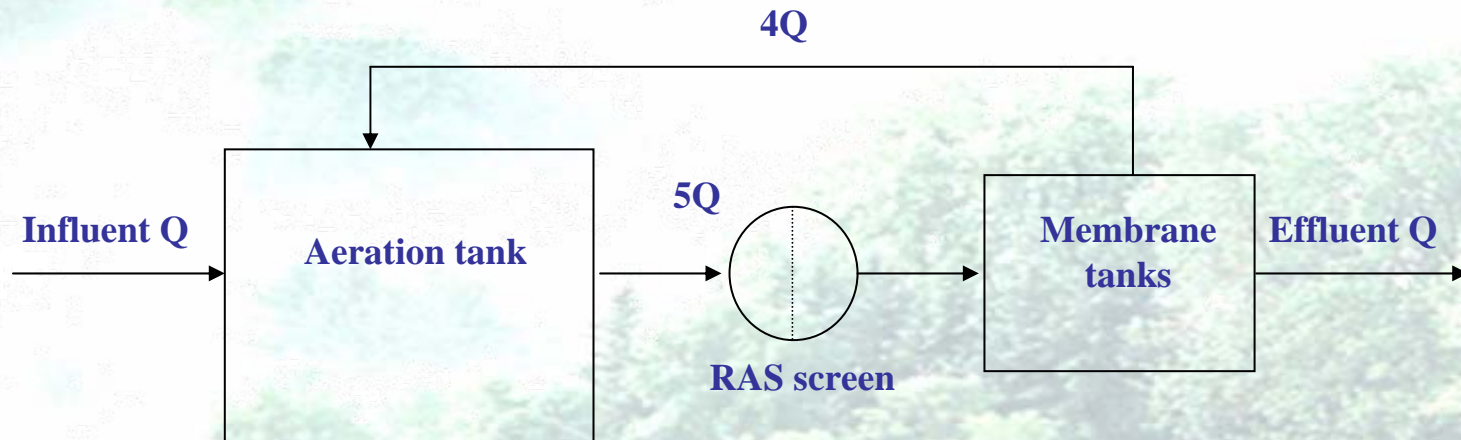
**Hollow Fibres**



**Flat Sheet**

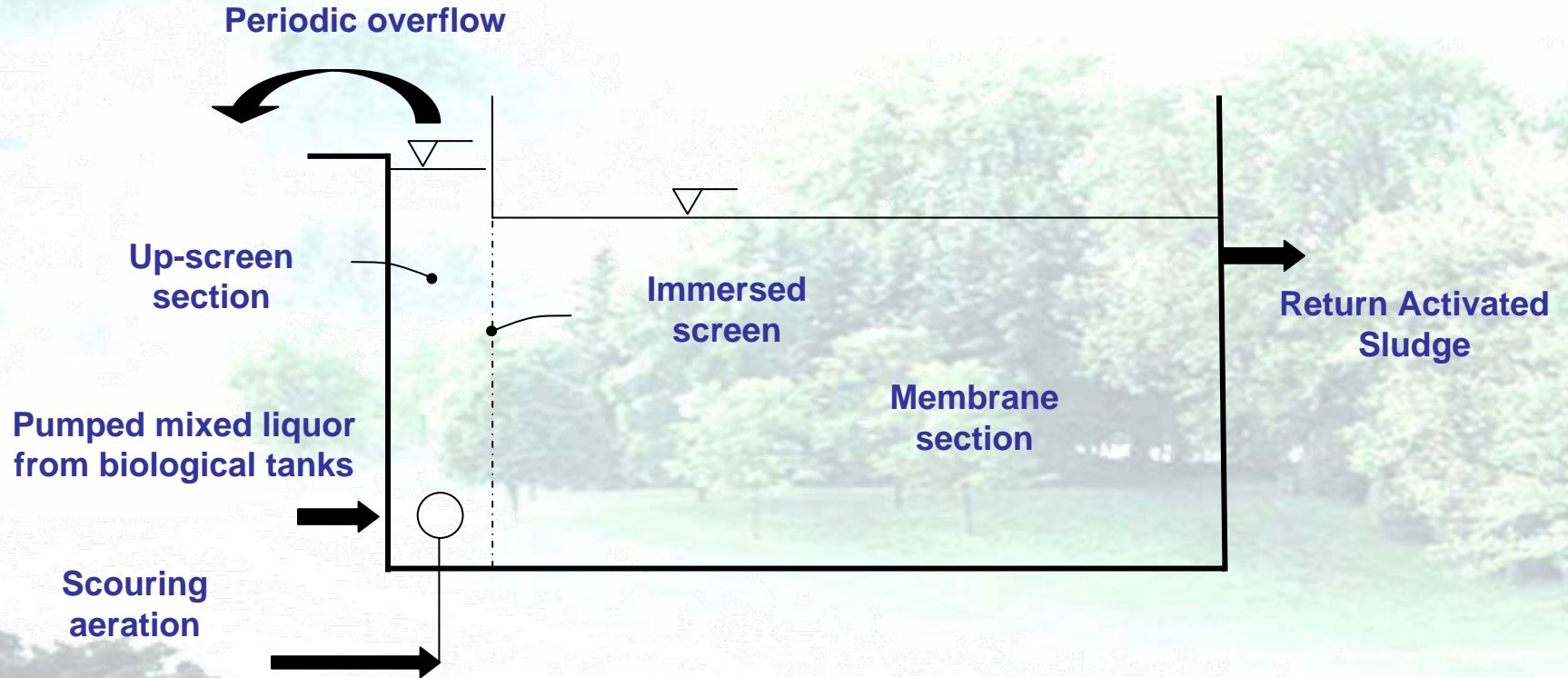


# Full RAS Flow Screening



- ❑ Only option to positively protect the membranes from trash in the feed and contamination downstream of head-works
- ❑ Possibility to relax head-works screening requirements
- ❑ Trash remain in the aeration tank and can be extracted with the waste activated sludge

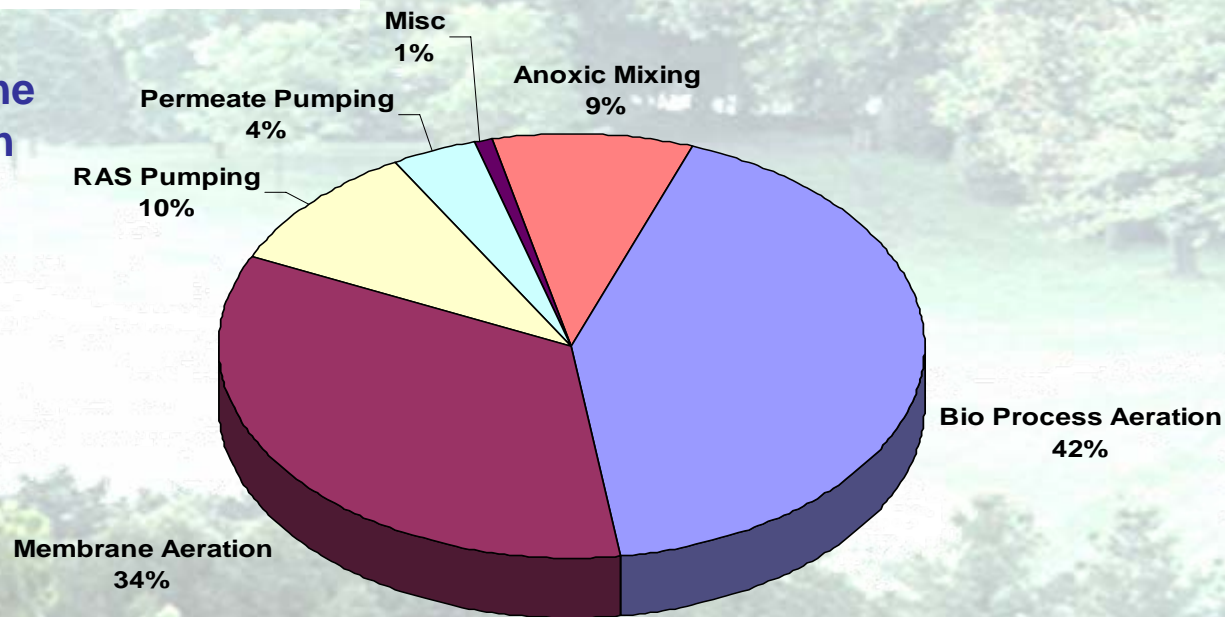
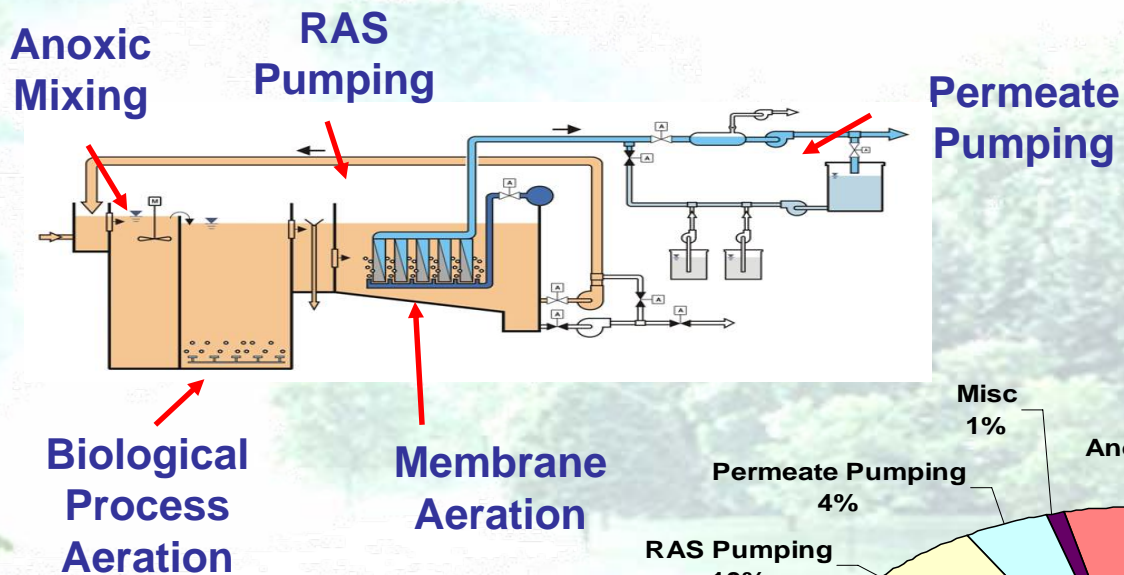
# Immersed Screen Concept



# 7 The Use of Air for Scouring Membranes

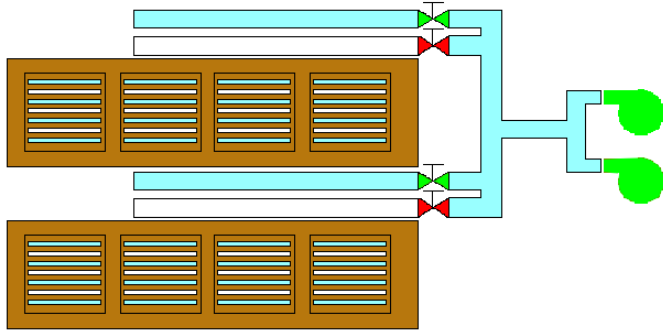
- Essential process feature with O/I hollow fibres
- Used only as part of back-wash sequence in low solids applications
- Used “continuously” in MBR applications
- Cyclic aeration to improve scouring performance and reduce energy consumption
- Coarse bubbles needed for scouring efficiency
- Little contribution to oxygen transfer in MBR

# MBR Energy Users (with 10/10 membrane aeration)

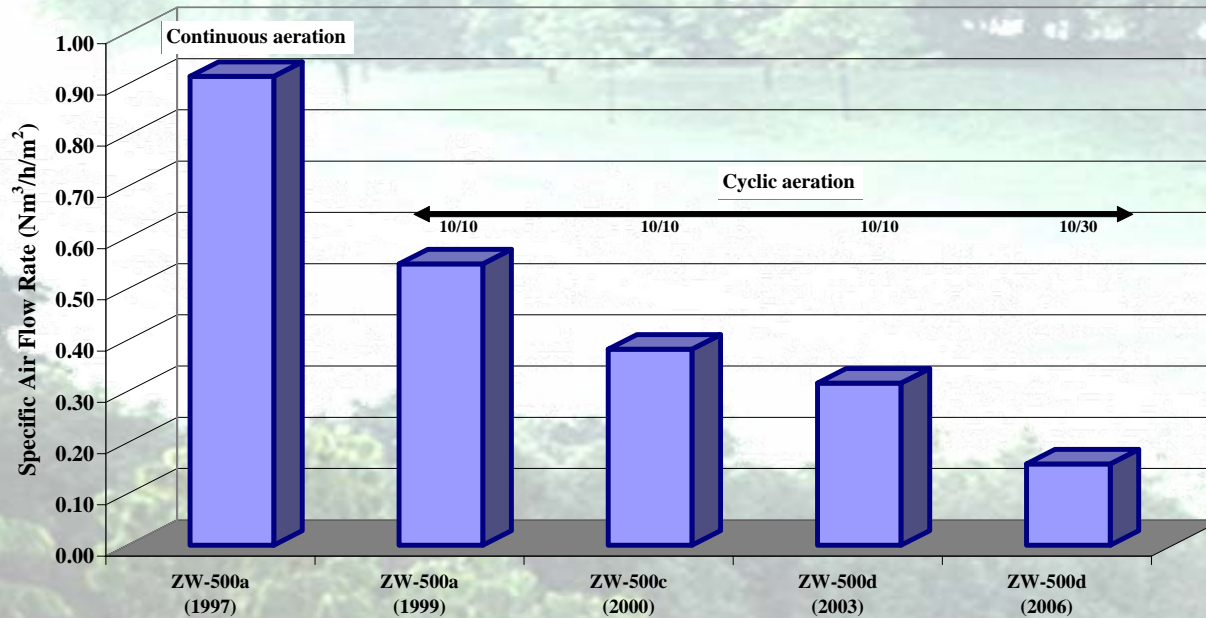
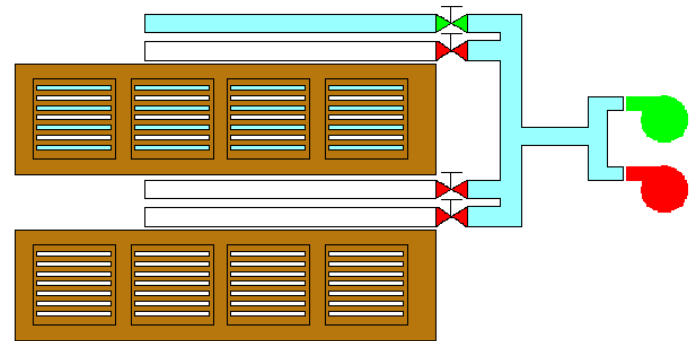


# Cyclic Aeration

10s on / 10s off



10s on / 30s off

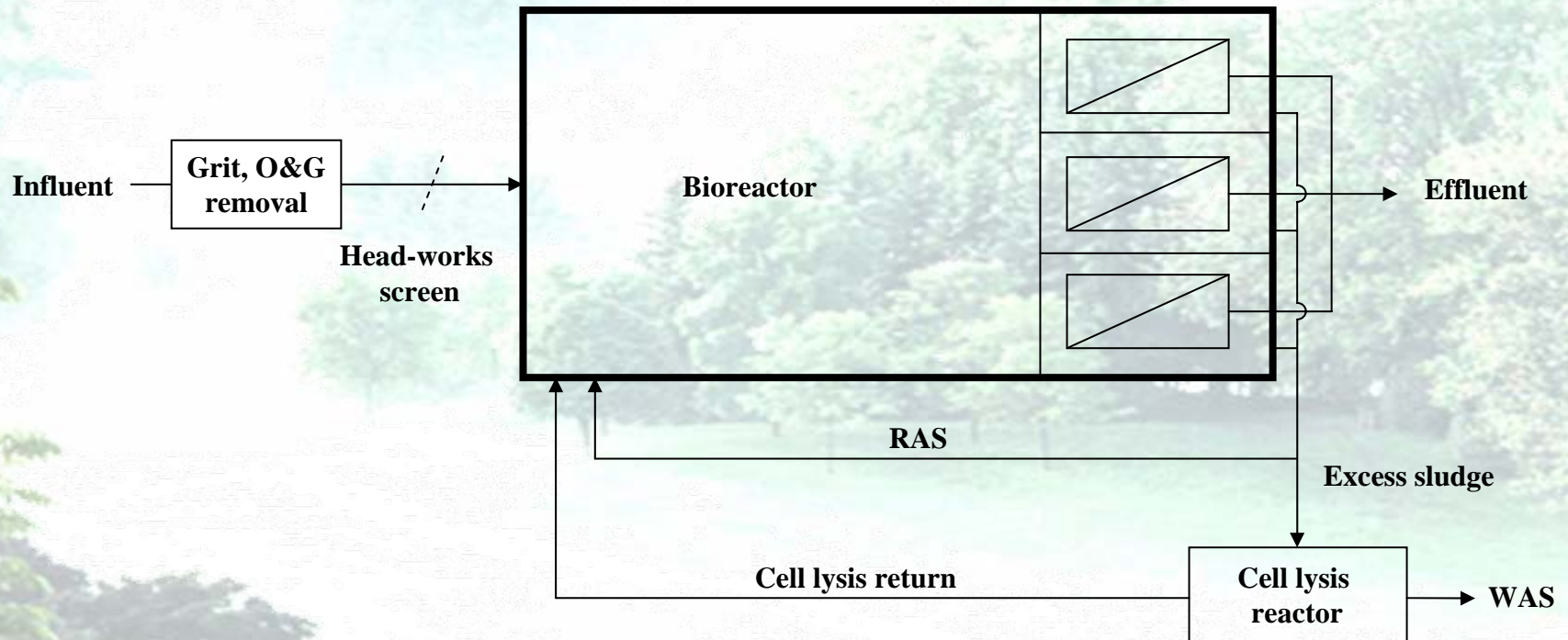




## 8) What to do with MBR residuals?

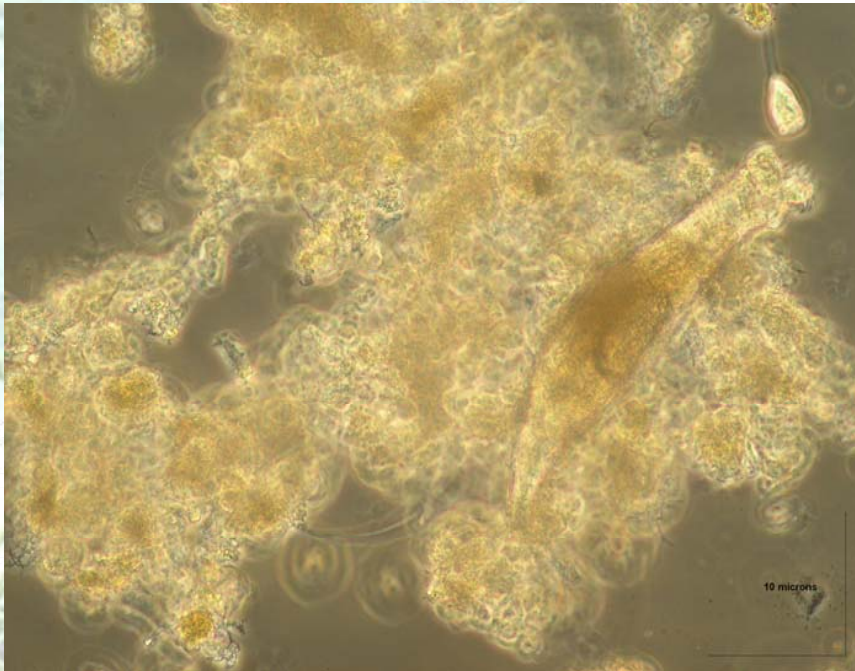
- Minimize their formation; is sludge reduction in the MBR feasible?
- Can low growing biomass be combined with MBR (attached growth, membrane-supported biofilm, aerobic granules)?
- An anaerobic MBR would offer low residuals with the potential of biogas production, but...

# Sludge Reduction Process Flow Diagram



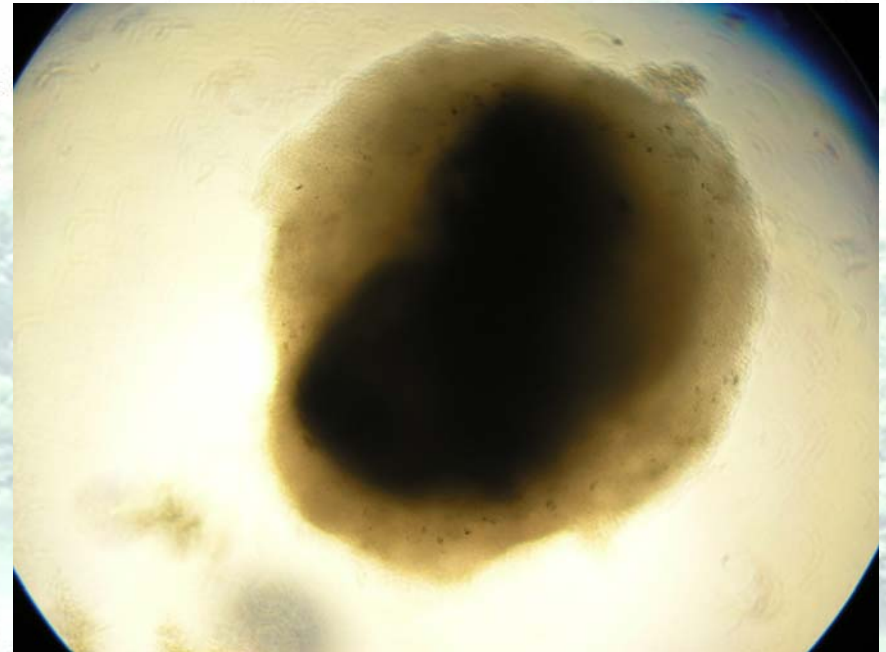
# Light flocs versus Aerobic Granules

**Light floc**



Settling velocity = 1-3 m/h

**Aerobic granule**



Settling velocity = 30 to 70m/h

# Membrane-Supported Bioreactor



50-80  $\mu\text{m}$  dense hollow fibres

Can fine hollow fibres be used for oxygen transfer and as a support for biomass?

Potential benefits:

- 4-5 fold reduction in aeration costs
- Low excess sludge
- Low suspended loading to final membrane separation step